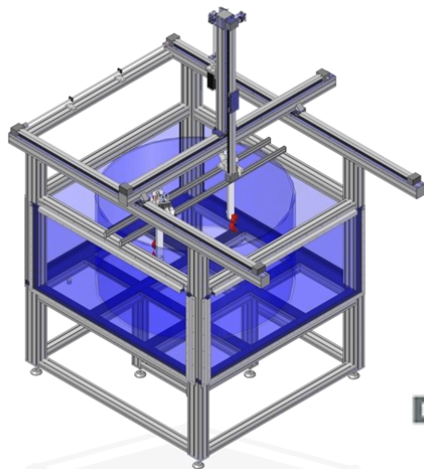


# Modellierung der Durchmischungsvorgänge im Fermenter für eine gezielte Optimierung der Rührwerke

Markus Kolano, Matthias Kraume

[markuskolano@gmail.com](mailto:markuskolano@gmail.com), [matthias.kraume@tu-berlin.de](mailto:matthias.kraume@tu-berlin.de)

Fachgebiet Verfahrenstechnik



 **Fraunhofer**  
IKTS



**Sens-O-Mix**

<https://www.fnr.de/index.php?id=11150&fkz=2219NR437>

  
**RTO**  
Repowering Technik Ost



  
**FNR**

Fachagentur Nachwachsende Rohstoffe e.V.



Bundesministerium  
für Ernährung  
und Landwirtschaft



Fachgebiet Verfahrenstechnik  
[www.vt.tu-berlin.de](http://www.vt.tu-berlin.de)

Biogas Infotage 2024, Ulm  
01.02.2024

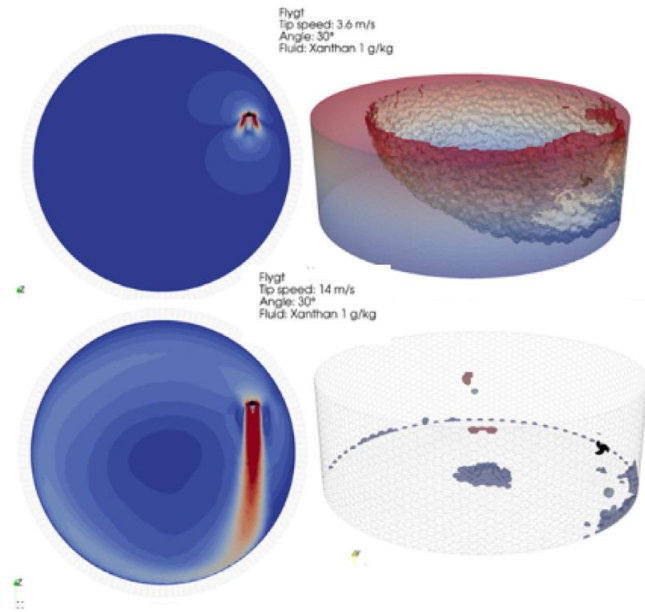
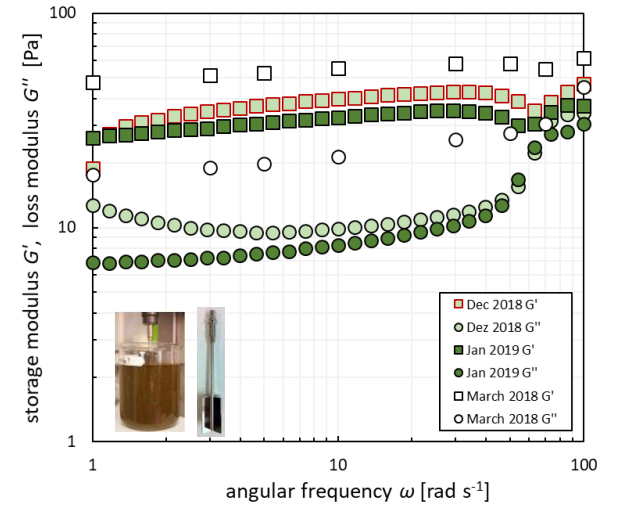
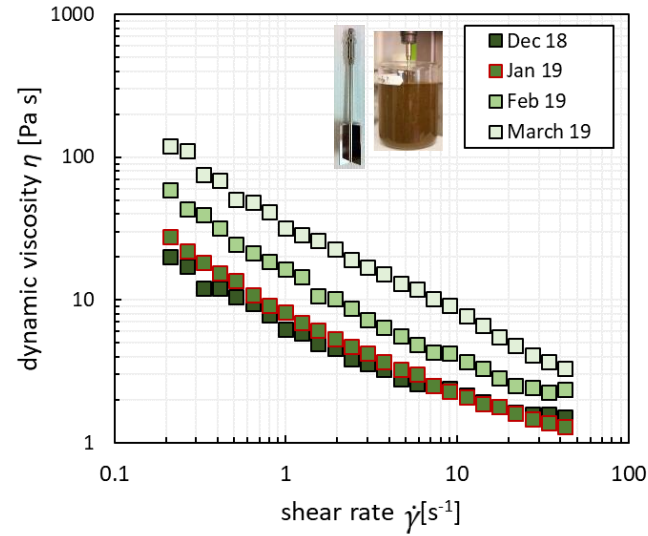


# Motivation – Agitating biogas fermenters

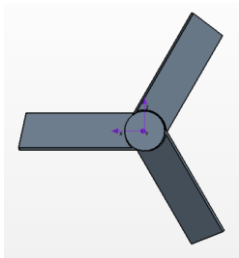
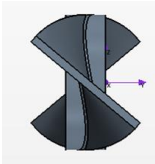
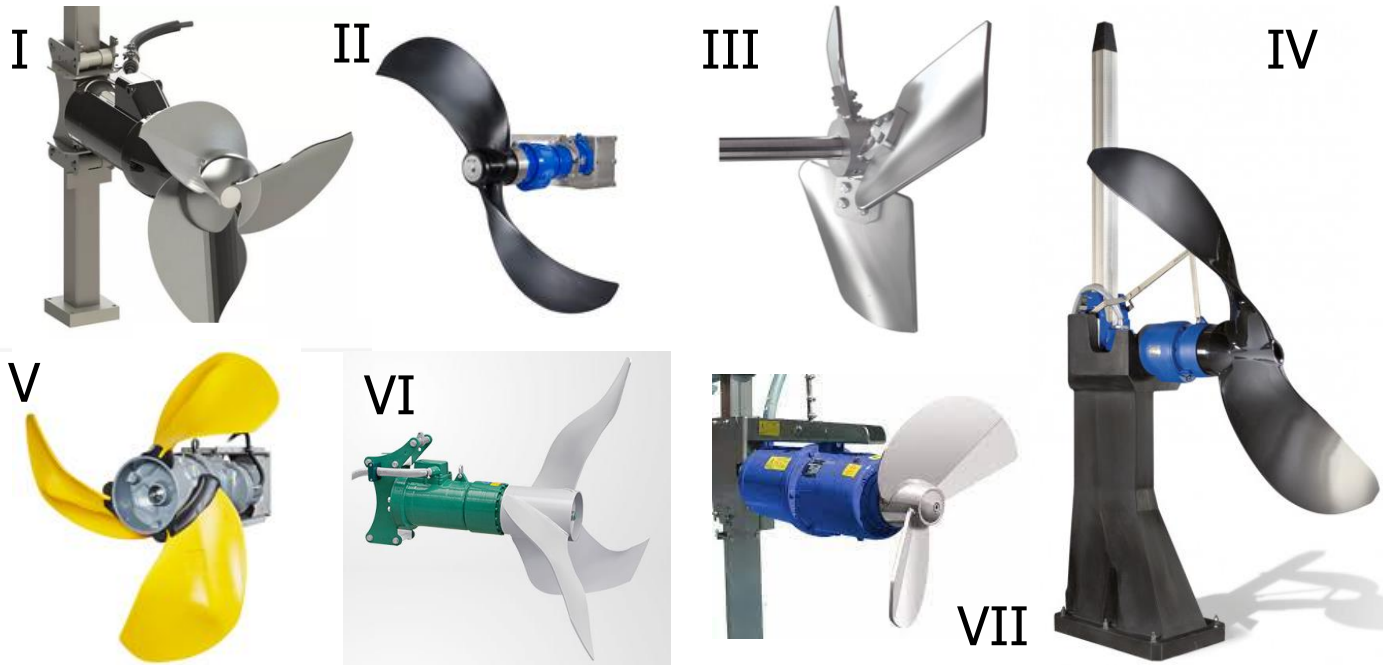
<http://www.rotaria.com/>



<http://www.dh1ply.de/riedlbauer547.html>

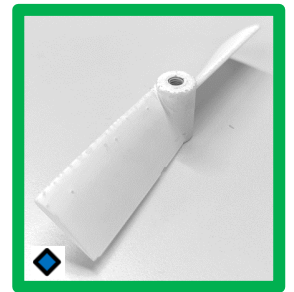


# Motivation – Agitating biogas fermenters



## How should an efficient biogas agitator be designed?

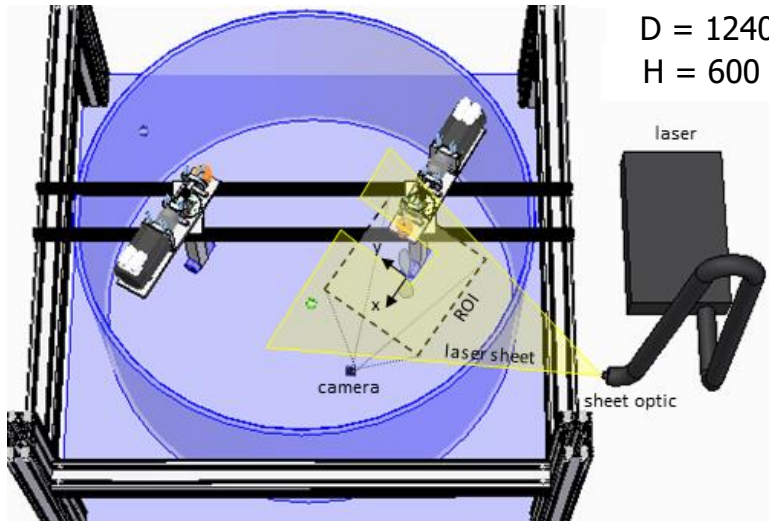
- **Experimental** study on propeller flows in non-Newtonian media
- Geometrical parameter study using **CFD**
- Validation using **3D-printed models**



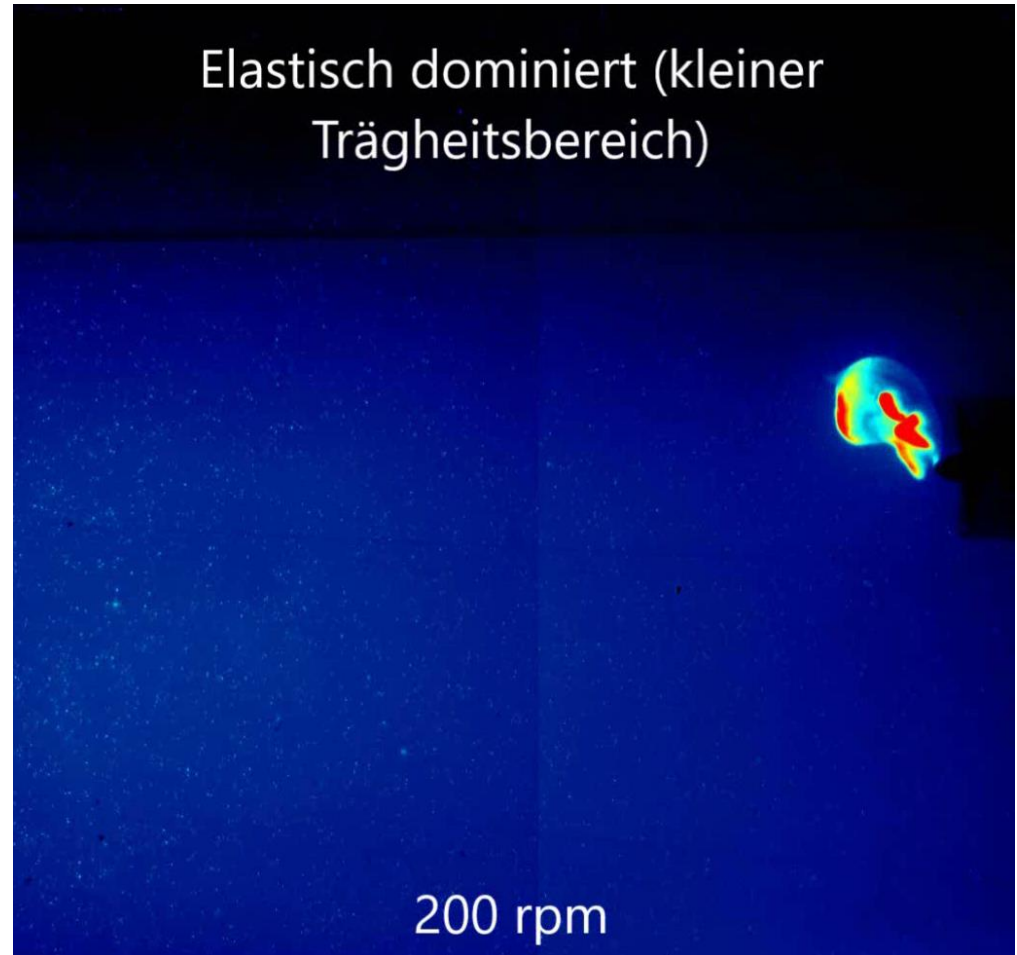
# Stirring experiments – Laser-induced fluorescence

Xanthan gum 1 g/kg

D = 1240 mm  
H = 600 mm



Elastisch dominiert (kleiner  
Trägheitsbereich)



d = 142 mm



d = 102 mm



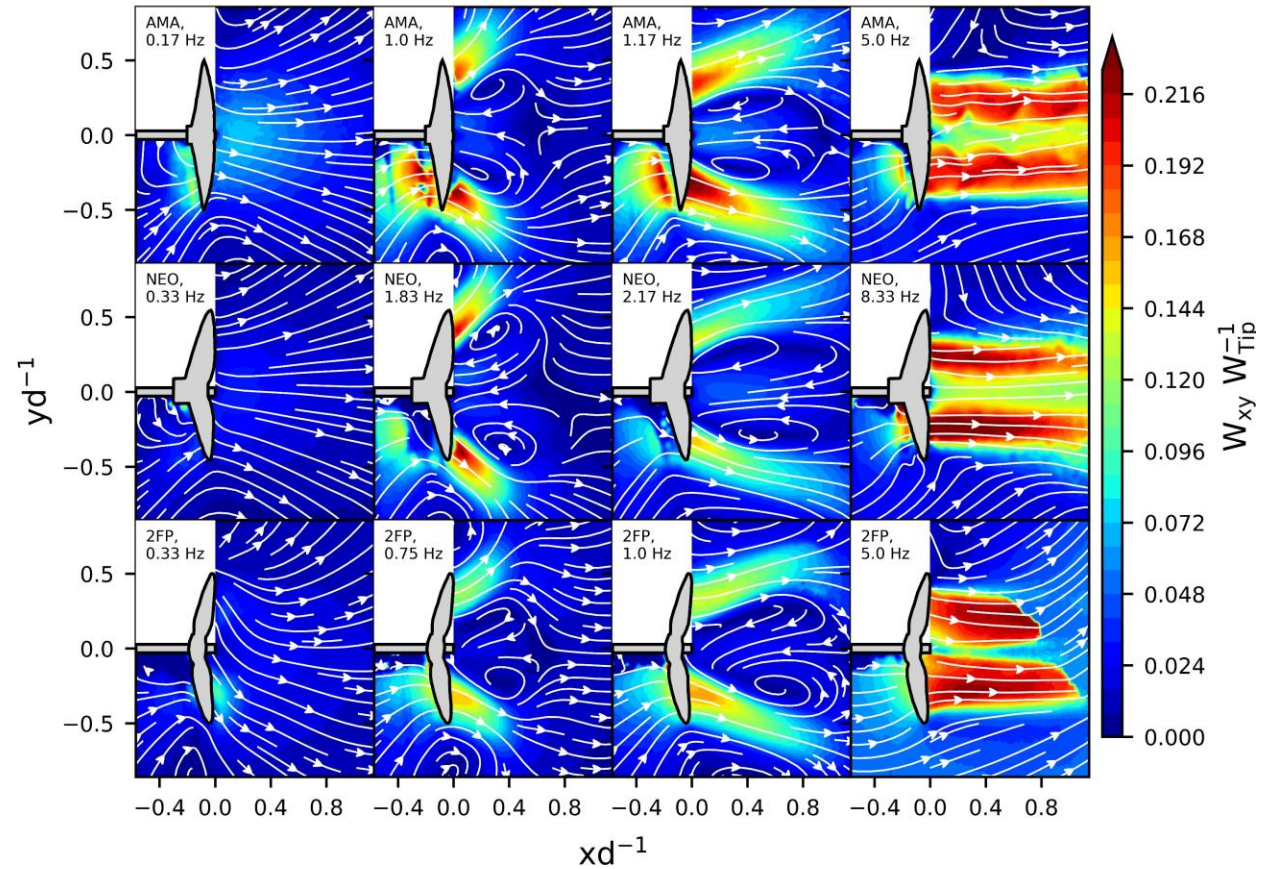
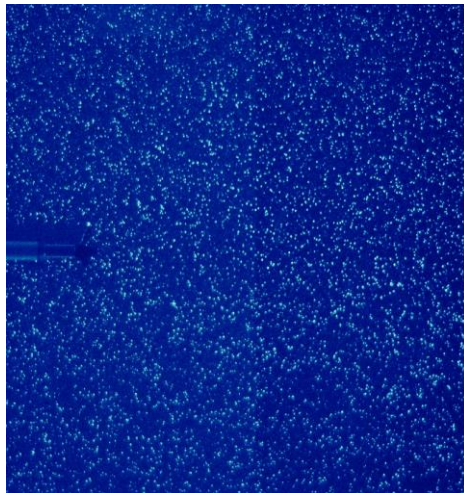
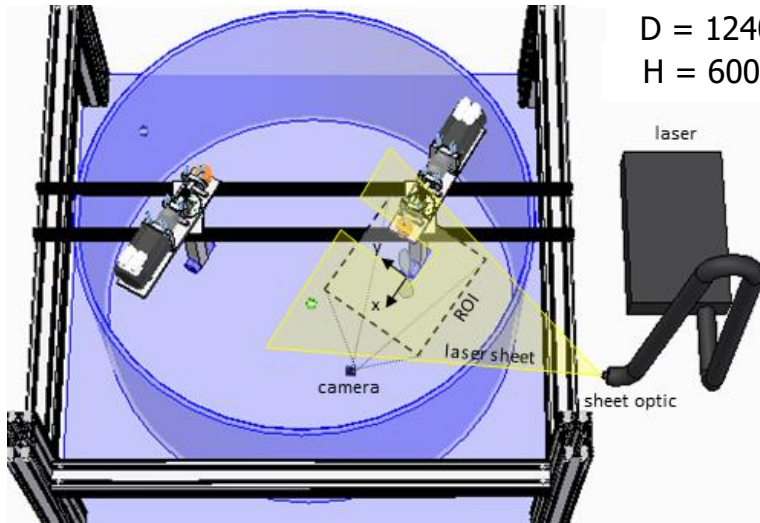
d = 175 mm

# Stirring experiments – Particle image velocimetry

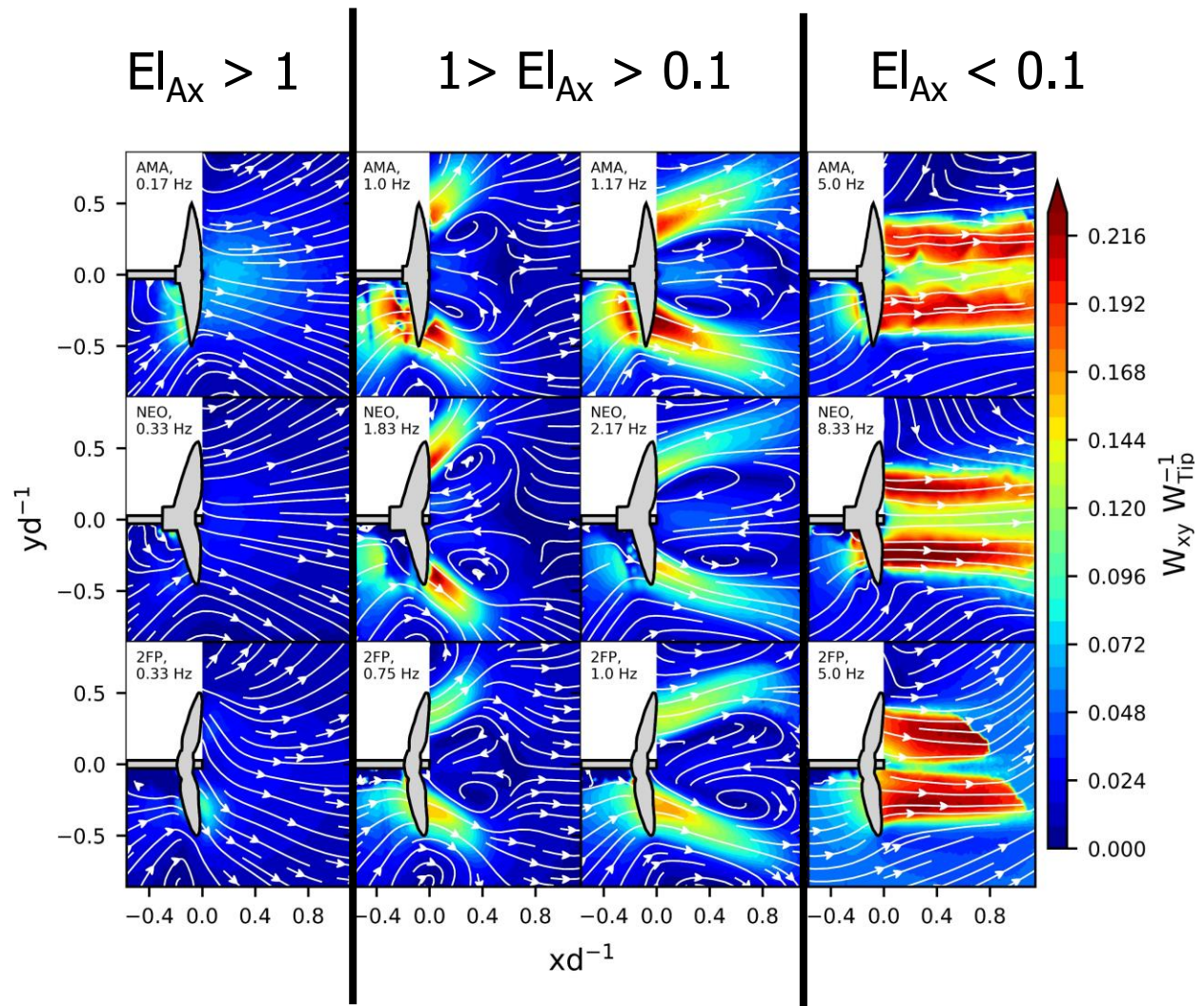
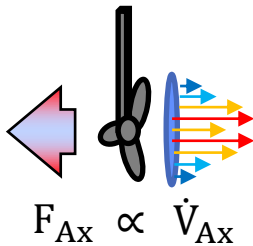
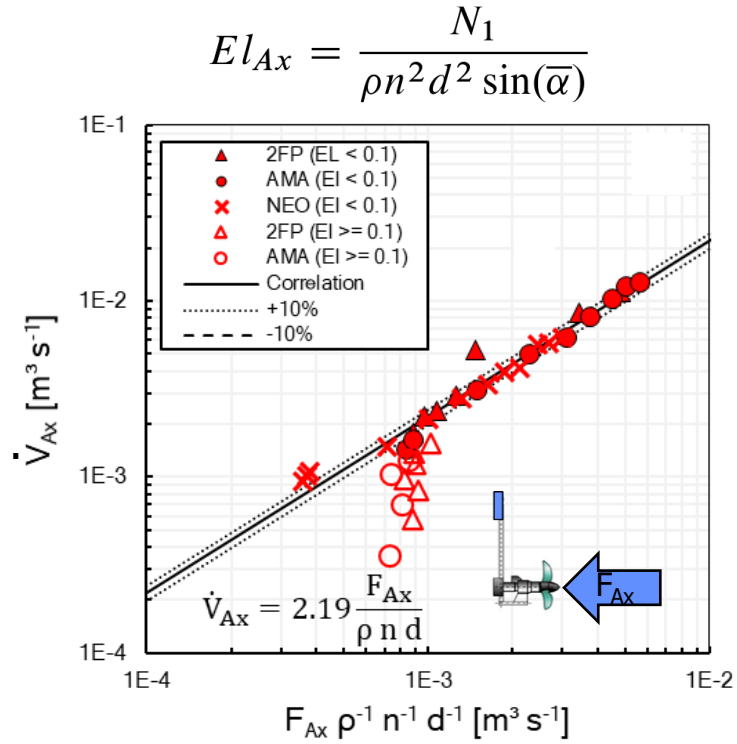
Xanthan gum 1 g/kg

$D = 1240 \text{ mm}$

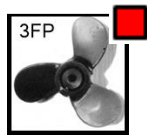
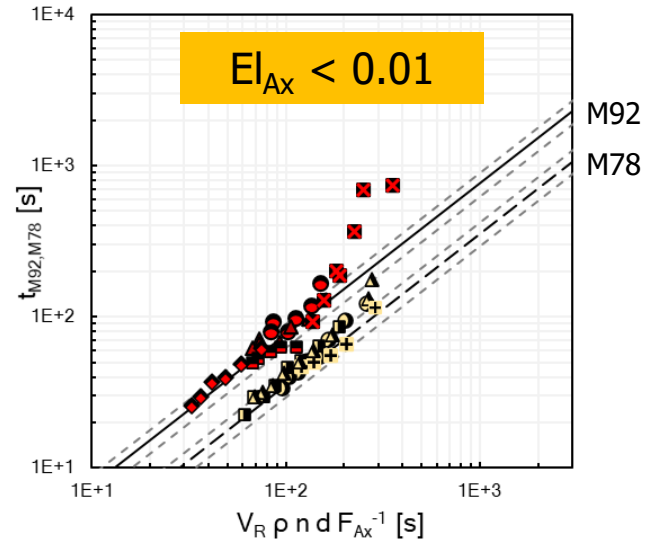
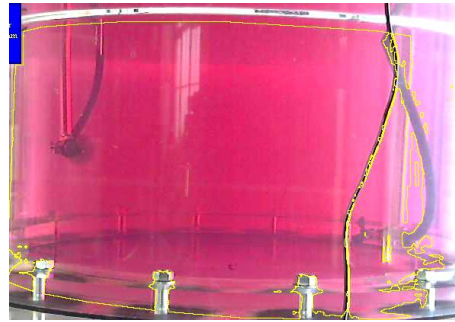
$H = 600 \text{ mm}$



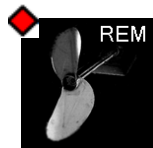
# Stirring experiments – Elasticity number and thrust correlation



# Stirring experiments – Thrust & mixing times



d = 130 mm



d = 155 mm



d = 175 mm



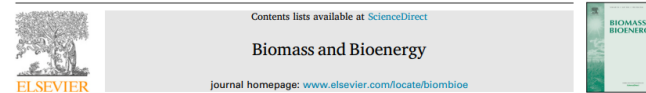
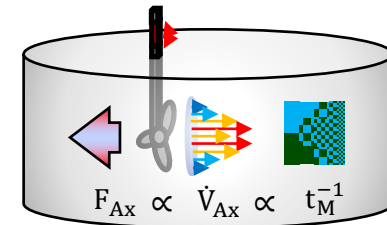
d = 102 mm



d = 142 mm

$$t_M = c_M V_R \frac{\rho n d}{F_{Ax}}$$

—  $c_M = 0.763$  for  $t_{M92}$   
 - -  $c_M = 0.356$  for  $t_{M78}$

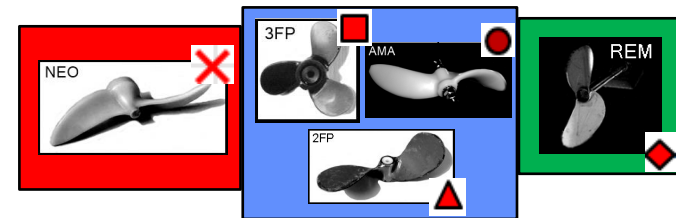
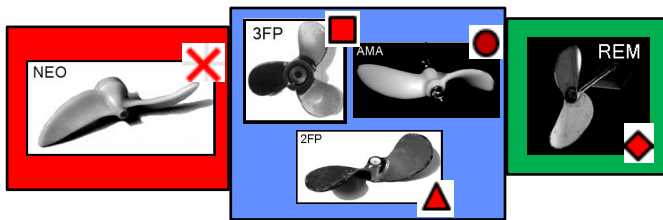
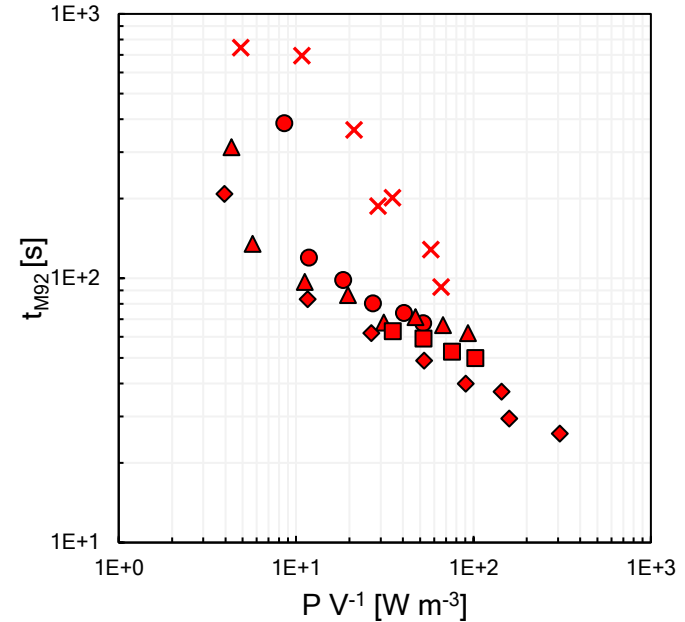
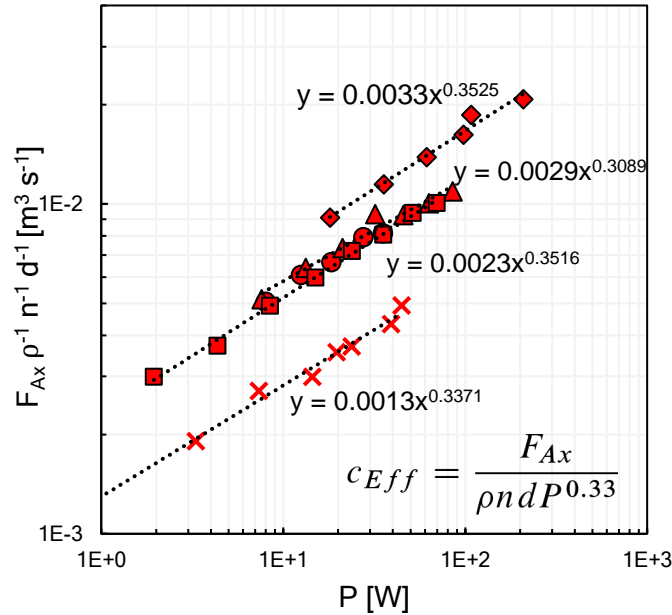


Research paper  
 Using thrust to control the mixing process in stirred tanks with side-entering agitators and viscoelastic fluids  
 M. Kolano\*, J. Danke, M. Kraume  
 Chair of Chemical and Process Engineering, Technical University of Berlin, Ackermannstraße 76, 13355 Berlin, Germany

# Agitator optimization – Experimental data / Target function

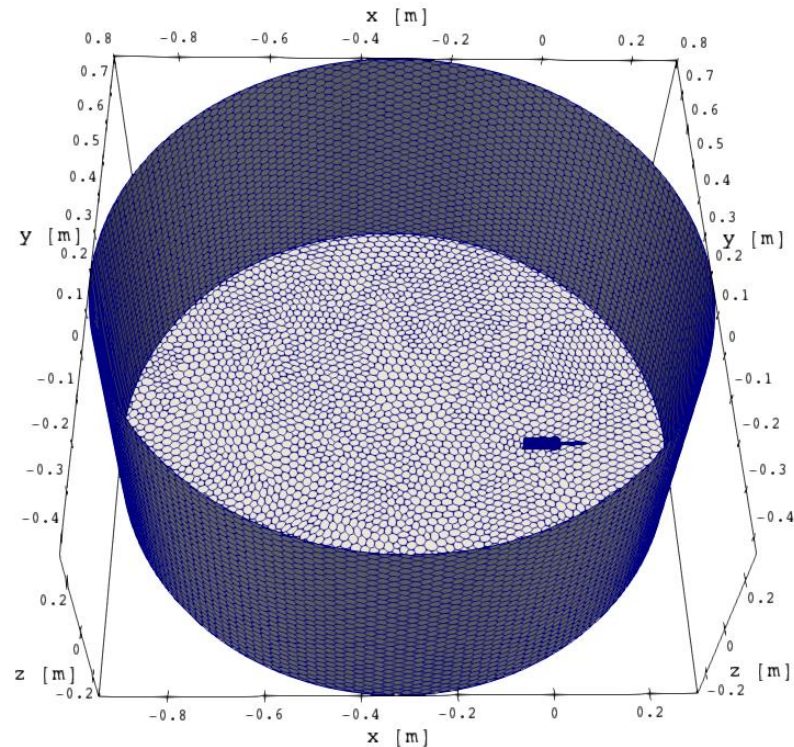
$$t_M = c_M V_R \frac{\rho n d}{F_{Ax}}$$

$$\max \left( \frac{\dot{V}}{P} \propto \frac{F_{Ax}}{\rho n d P} \right)$$





# Agitator optimization – CFD model



## Models/BC:

MRF (Rotating reference frame =  $300 \text{ rad s}^{-1}$ ;  $\text{Re} \approx 10^6$ )

K-omega turbulence model (low Re, no wall models)

Carreau-Yasuda viscosity

$$\eta = \eta_{\infty} + (\eta_0 - \eta_{\infty}) (1 + (\lambda\dot{\gamma})^a)^{(n-1)/a}$$

$$\eta_{\infty} = 10^{-3} \text{ Pa s}$$

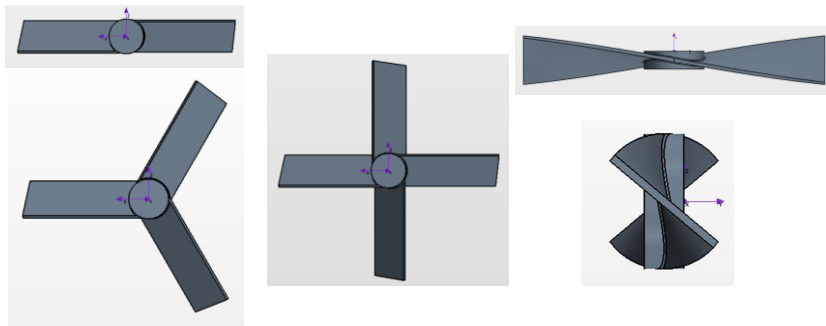
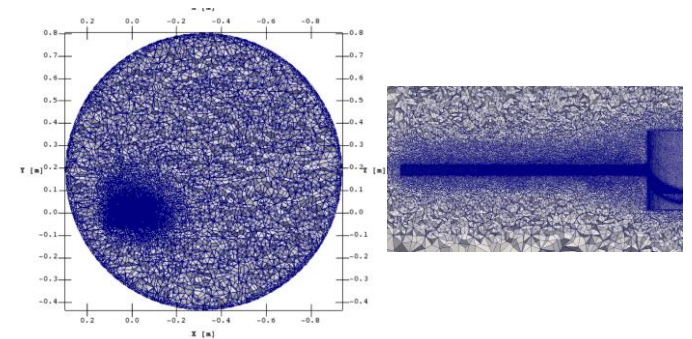


## Domain:

Ca. 2.5 Mio polyhedrals per blade

10 Prims layers (growth rate 1.3)

$Y^+ \approx 1$



$d = 130 \text{ mm}$ ;  $h = d/5$ ;  $w = 3 \text{ mm}$

## Solver:

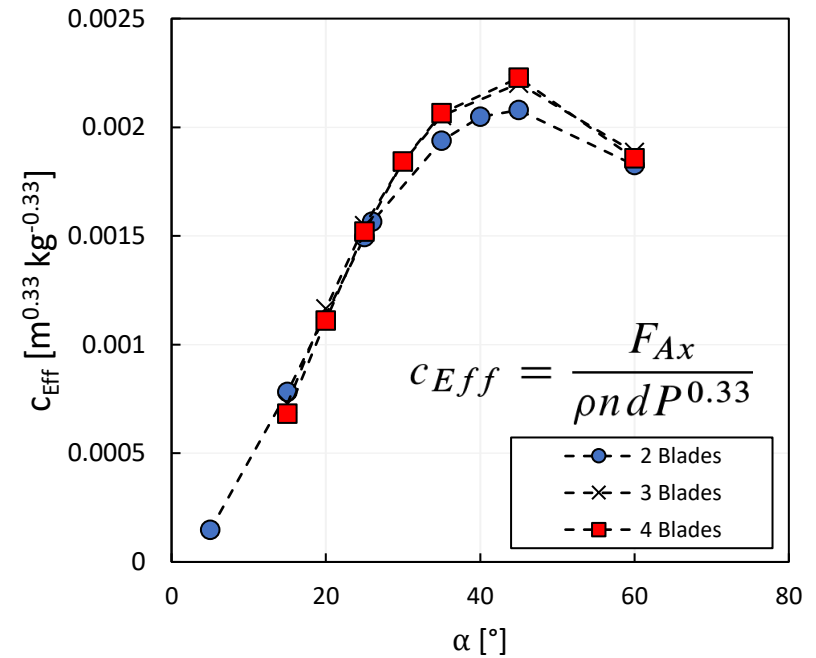
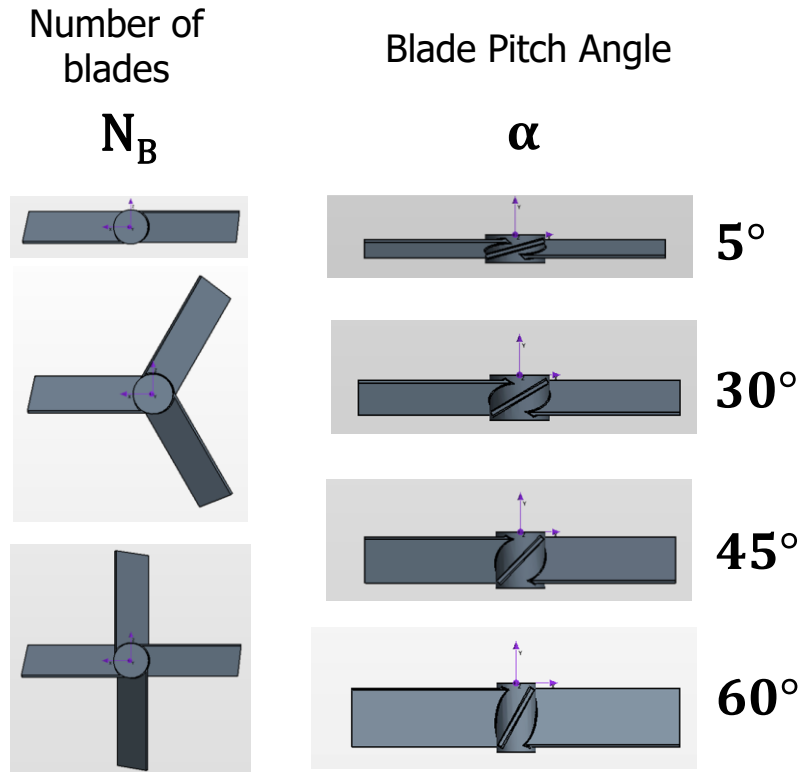
SIMPLE (steady state, OpenFOAM v2012)

10000 Iterations (Relaxation  $p=0.3$ ,  $U=0.7$ ,  $k/\omega=0.5$ )

Convergence:  $10^{-5}$  for each property

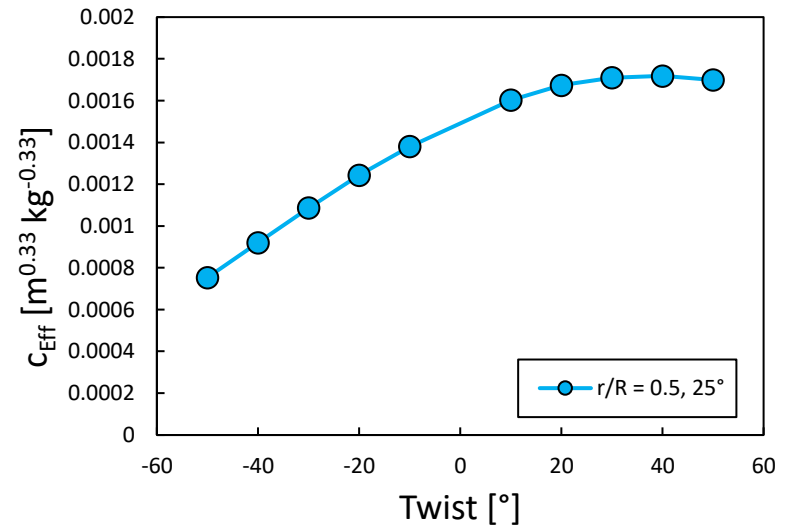
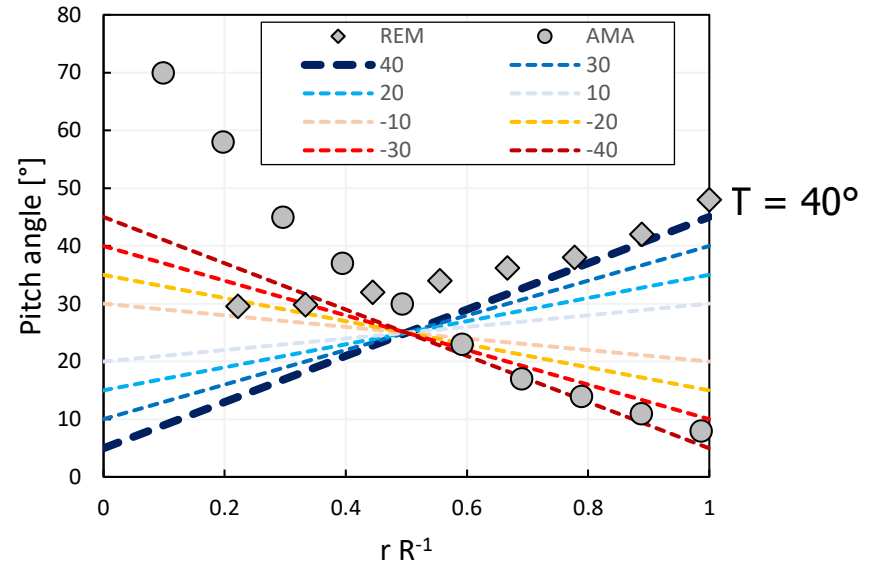
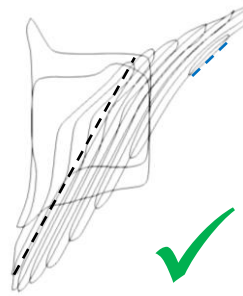
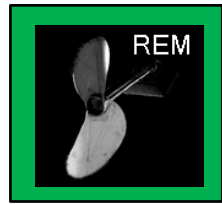
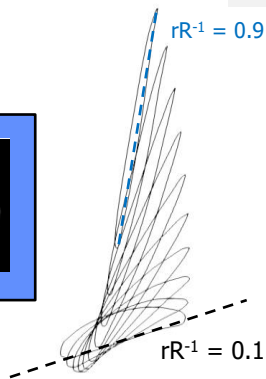
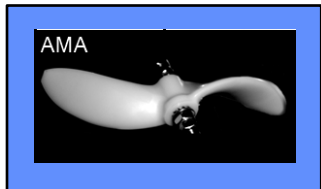
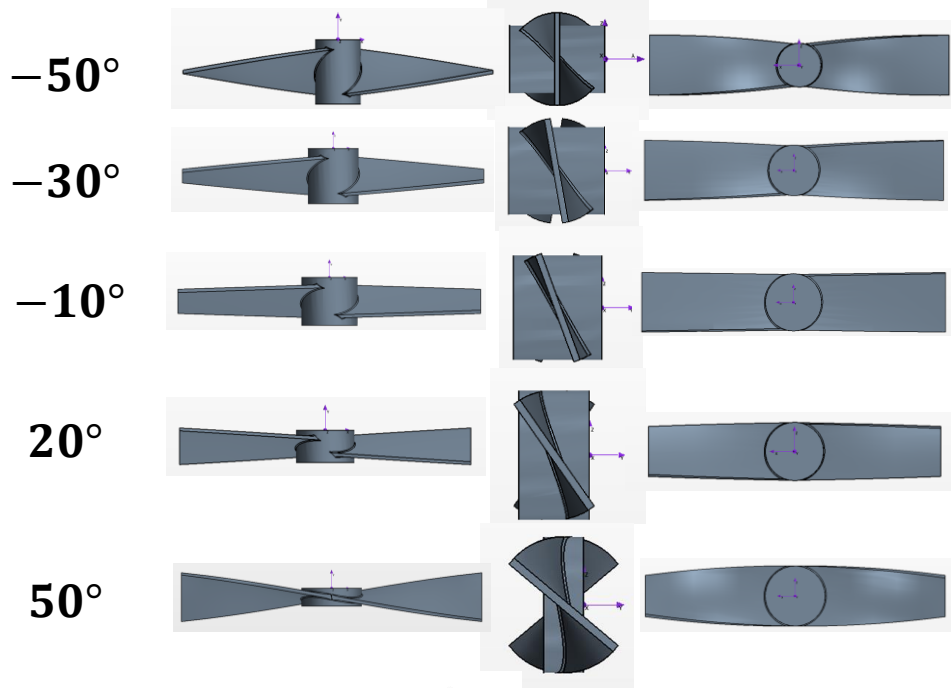
→ not reached due to transient effects in turbulence modeling, but deviation less than 5% from mean and periodic (tested by transient MRF simulation)

# Agitator optimization – Number of blades and pitch angle



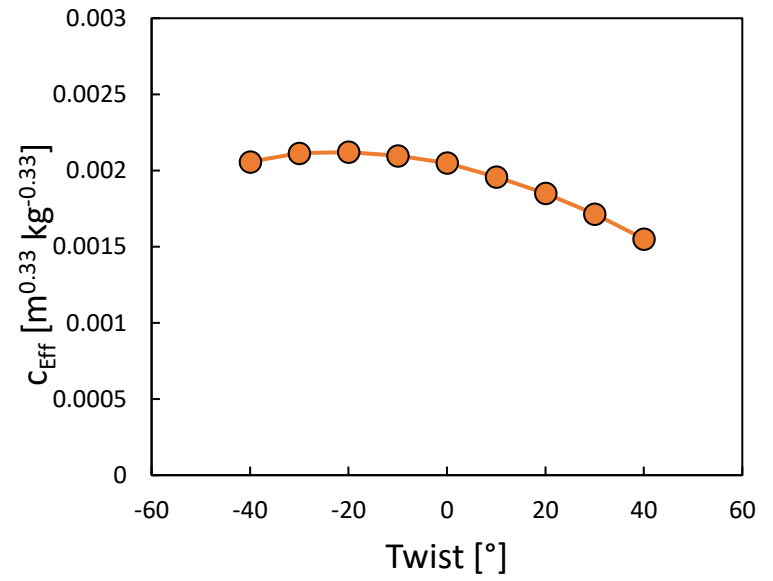
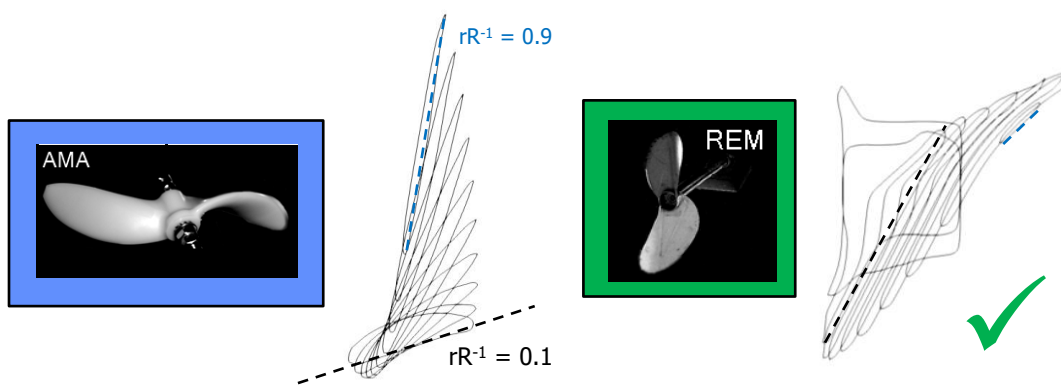
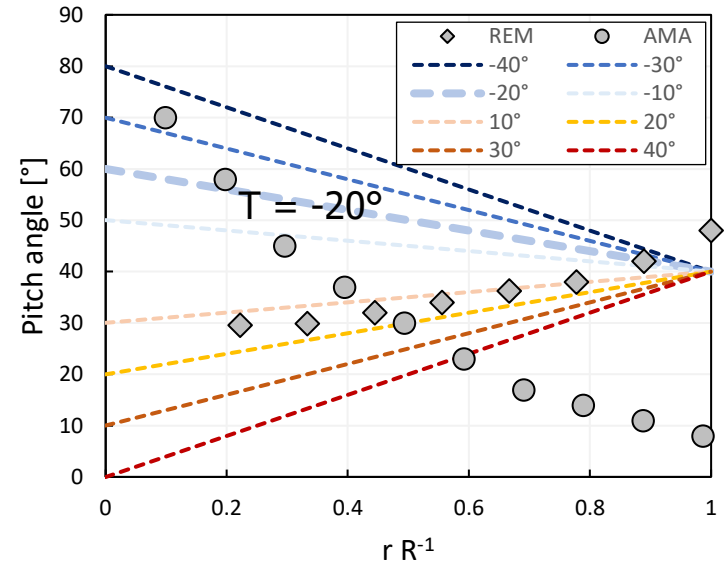
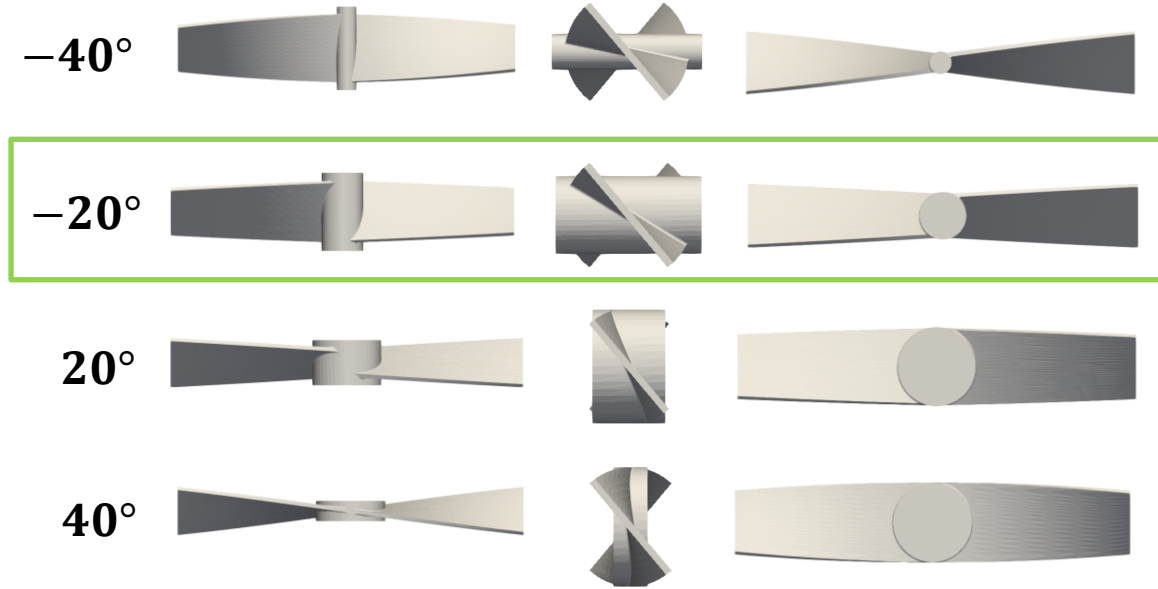
# Agitator optimization – Blade twist

Blade twist  $T$



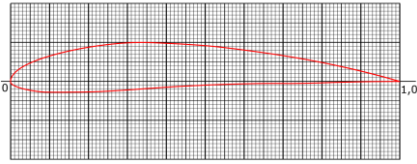
# Agitator optimization – Blade twist

Blade twist  $T$

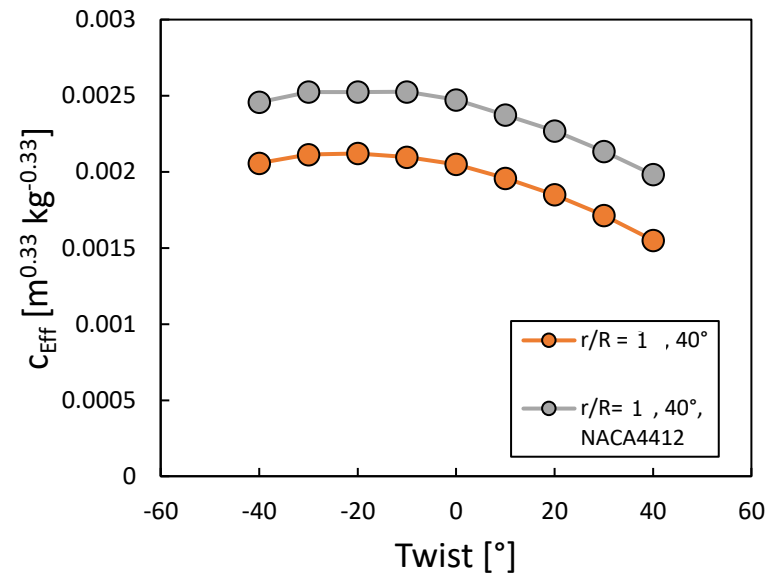
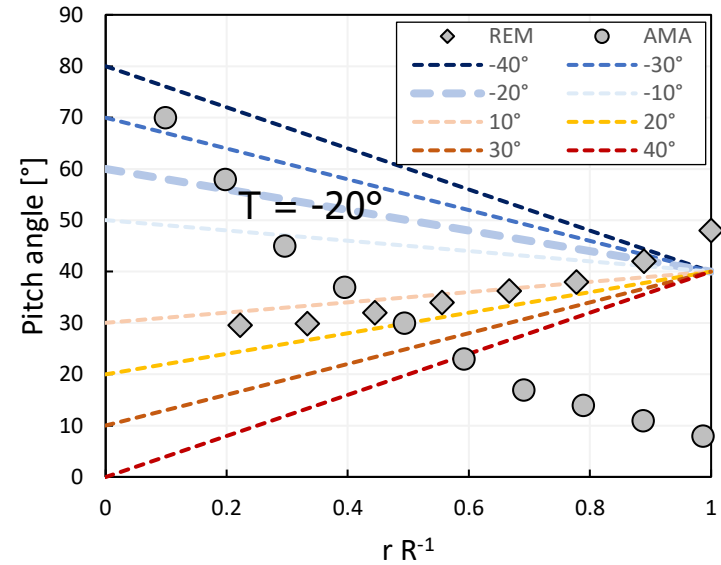
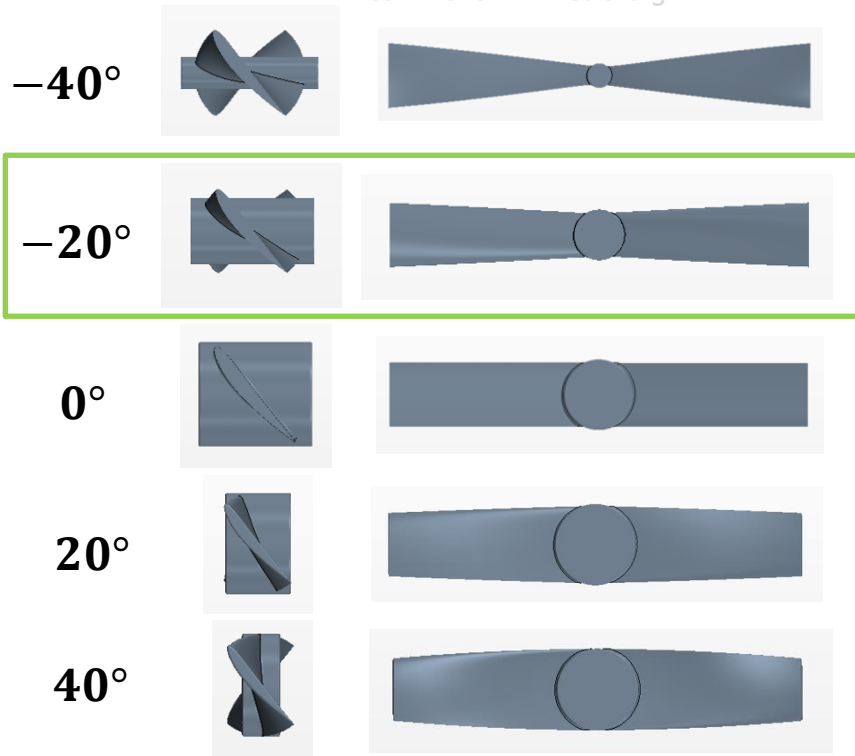


# Agitator optimization – Blade twist + NACA4412

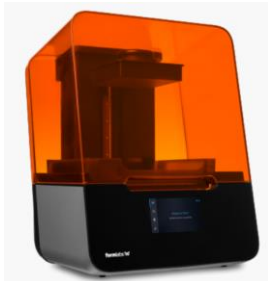
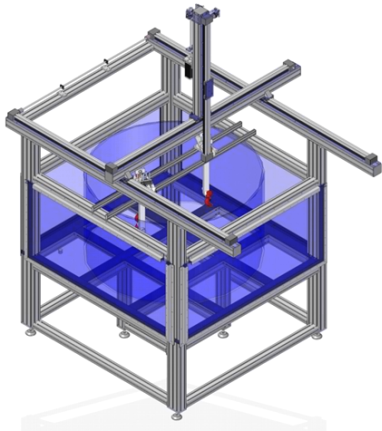
## NACA 4412



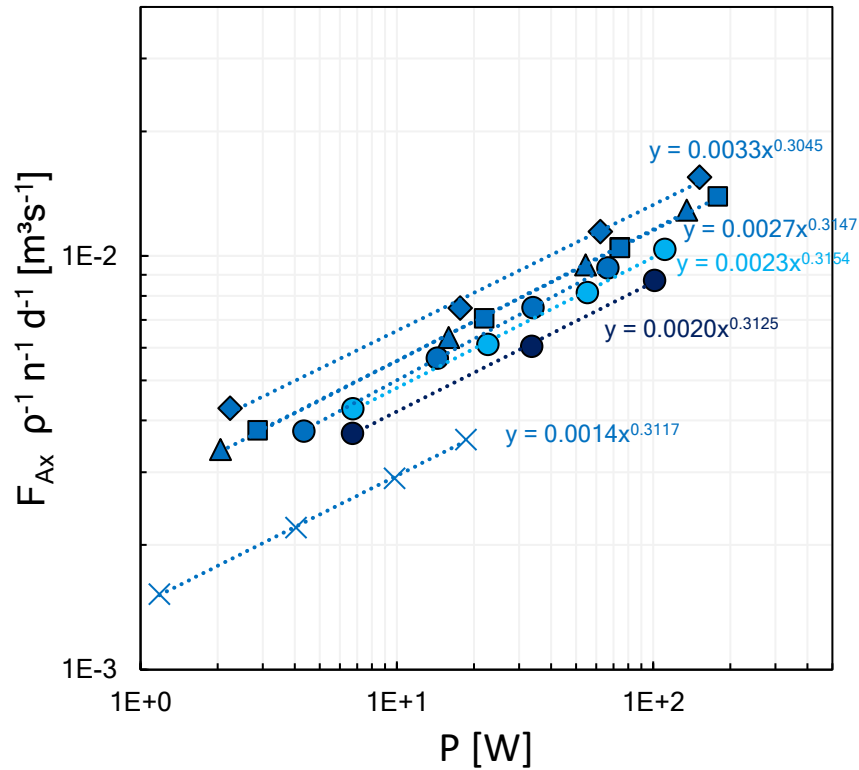
commons.wikimedia.org



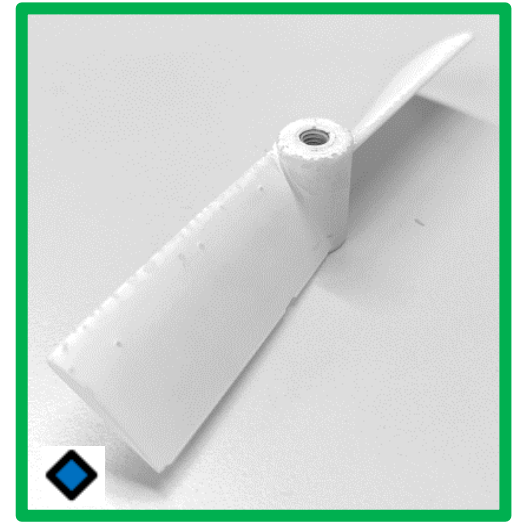
# Agitator optimization – 3D-printed models



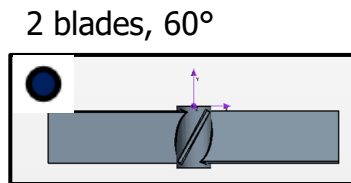
formlabs.com



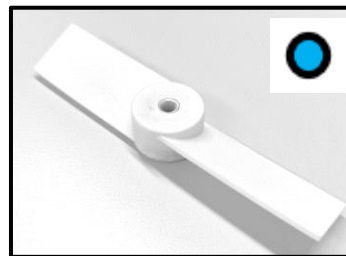
2 blades, 40°,  
NACA4412,  
Twist -20°



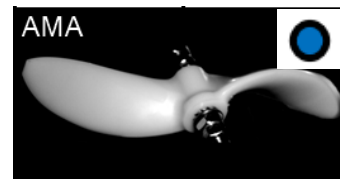
NEO



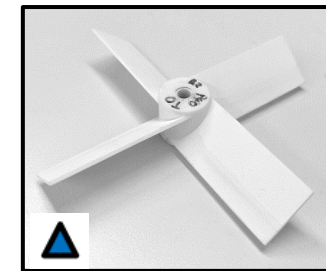
2 blades, 60°



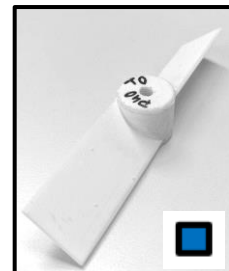
2 blades, 25°



AMA



4 blades, 40°

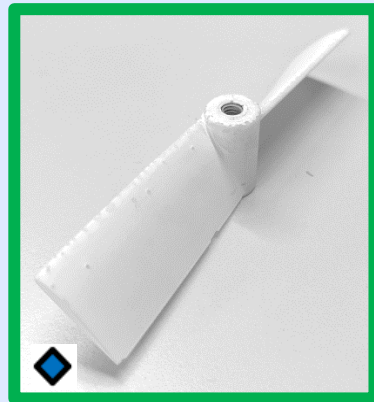
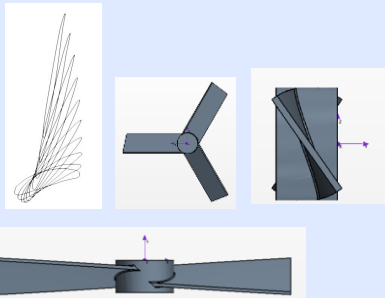


2 blades, 40°

# Summary / Outlook

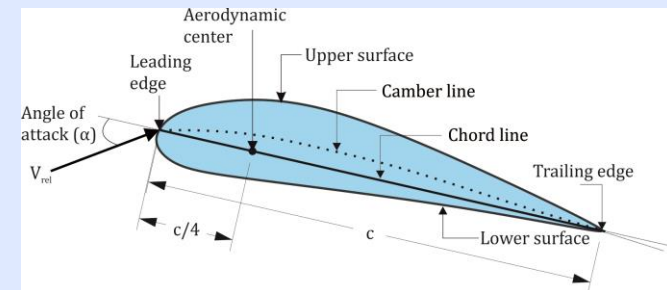
## Summary

- Target function for efficient side-entry propeller design
- Geometrical optimization:
  - Optimal pitch angle  $45^\circ$
  - Number of blades of minor importance
  - Pitch angle at  $r/R=1$  most important
  - Hydrofoils improve efficiency distinctly
  - CFD results validated by experiments



## Outlook

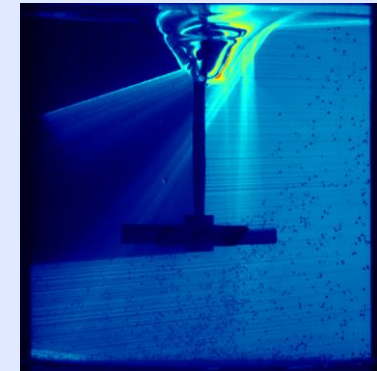
### Hydrofoil



### Propeller hub

### Stability / Fibers

### Suspension



---

# Thank you for your attention!



Bundesministerium  
für Ernährung  
und Landwirtschaft

Sources:

I: <https://zorg-biogas.com/>

II: <https://repowering-technik-ost.de/ruehrwerke/>

III: <https://www.spxflow.com/lightnin/products/a312-medium-solidity-hydrofoil-impeller/>

IV: <https://www.ksb.com/>

V: <https://www.xylem.com/en-US/brands/flygt/>

VI: <https://www.suma.de/>

VII: <https://www.bauer-at.com/>



Fachagentur Nachwachsende Rohstoffe e.V.



Fachgebiet Verfahrenstechnik  
[www.vt.tu-berlin.de](http://www.vt.tu-berlin.de)

Biogas Infotage 2024, Ulm  
01.02.2024

